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Patentanmeldung Nr. PCT/EP 02/44565
Patent application no.
Demande de brevet n°

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Blatt 2 der Bescheinigung
Sheet 2 of the certificate
Page 2 de l'attestation



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Application no.:
Demande n°:

PCT/EP 02/14565 ✓

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PROCESS FOR PRODUCING A TYRE FOR VEHICLE WHEELS

The present invention relates to a process for producing a tyre for vehicle wheels.

5 More in particular, the present invention relates to a process for producing a tyre for vehicle wheels which includes: feeding an elastomeric composition to an extruder; forming by extrusion said elastomeric composition as a continuous elongated element; depositing
10 said continuous elongated element on a rigid support in a plurality of coils to make up a structural element of a tyre.

The present invention also relates to a method for reducing the elongational viscosity of an elastomeric
15 composition.

The manufacture of tyres for vehicle wheels involves the formation of a carcass structure essentially made up of one or more carcass plies substantially of a toroidal shape and having their axially opposite side edges in
20 engagement with respective circumferentially inextensible annular reinforcing elements, usually referred to as "bead wires".

On the carcass structure is applied, in a radially external position, a belt structure comprising one or
25 more belt strips in the form of a closed ring and essentially made up of textiles or metallic cords suitably oriented with respect to each other and with respect to the cords belonging to the adjacent carcass plies.

30 At a radially external position of the belt structure, a tread band is provided which usually consists of a band of elastomeric material of suitable thickness.

Finally, a pair of sidewalls is provided on the
35 opposite sides of the tyre, each of said sidewalls covering a side portion of the tyre included between a so-called shoulder region located in proximity to the

corresponding side edge of the tread band, and a so-called bead located in correspondence to the respective bead wire.

Traditional production methods essentially provide
5 for the above listed tyre structural elements to be first made separately from each other, then to be assembled during a tyre manufacturing.

Many efforts have been recently made to reduce or possibly eliminate production and storage of semi-
10 finished products in a process for producing tyres.

In this regards, production processes have been proposed which aimed at obtaining given tyre structural elements such as tread band, sidewalls or others, by laying down a continuous elongated element of elastomeric
15 material of a reduced section with respect to that of the structural element to be obtained, on a rigid support bearing the tyre being manufactured, which elongated element is such arranged so as to form a plurality of consecutive coils disposed in side by side and/or
20 superposed relationship so as to define the structural element in its final configuration. Said rigid support may have a toroidal shape.

For example, WO 01/36185 in the name of the same Applicant, describes a method for manufacturing
25 elastomeric material components of a tyre for vehicle wheels comprising the steps of: feeding a continuous elongated element from a delivery member (e.g. an extruder) positioned adjacently to a toroidal support to apply said elongated element onto the toroidal support
30 itself; giving to the toroidal support a rotatory circumferential distribution motion about its own geometric rotation axis, so that the elongated element is circumferentially distributed on the toroidal support; carrying out controlled relative transverse distribution
35 displacements between the toroidal support and the delivery member to form with said elongated element a structural element of a tyre defined by a plurality of

coils laid down mutually approached and/or superimposed according to a pre-determined cross section profile to be conferred to said structural element. In particular said document teaches that if the peripheral speed of the toroidal support at the point of application of an elongated element is such controlled that a conveniently higher value than the feeding speed of the elongated element itself by the delivery member is maintained, adhesion of the applied elongated element is greatly improved and important advantages in terms of operating flexibility are achieved.

EP 0 968 814 describes a process and an apparatus for laying down rubber materials for tyre-constitutional members. A rubber material for a tyre-constitutional member is laid down on a rotating support with high efficiency and high accuracy by arranging a pair of rollers rotating in opposite directions in the vicinity of a radially outer surface portion of the support and utilising a gap defined between the rollers as a roller die. The apparatus for laying down rubber materials for tyre-constitutional members around a rotating support comprises a volumetric extruder for feeding an uncured rubber material on the rotating support, a pair of rollers located near to an outlet port of the volumetric extruder and near to a radially outer portion of the rotating support and driven in opposite directions to each other, and a gap defined between the pair of rollers and serving as a die for the rubber material to be laid down.

US 4 963 207 and US 5 171 394 disclose a method and apparatus for manufacturing tyres by the laying of rubber products on a firm rotatable support. The rubber products forming part of the tyre structure are laid down on a rigid core by means of a volumetric extruder having an outlet orifice of small size positioned close to the surface on which the rubber is applied. The rubber products are built up by a meridian displacement of the

orifice relative to the receiving surface with the extrusion of controlled volume of rubber.

However, prior art methods for manufacturing a tyre or making a tyre component by deposition of elastomeric elongated elements on a rigid support, present some
5 drawbacks.

In particular, Applicant has noticed that if the extrusion of said elastomeric elongated elements is carried out at a high shear rate (e.g. 1000 s^{-1}), the
10 obtained elastomeric elongated elements present some drawbacks such as, for example, irregular edges (e.g. ragged edges) and rough surfaces, premature crosslinking phenomena (scorching), which negatively affect the lay down of the same on a rigid support. More in particular,
15 Applicant noticed that said drawbacks are more evident in the case of elastomeric elongated elements comprising an elastomeric composition having a high Mooney viscosity ML(1+4) (e.g. higher than 70 at 100°C).

The Applicant tried to improve the processability of
20 said crosslinkable elastomeric composition by adding a plasticizer or a processing aid in order to decrease Mooney viscosity ML(1+4). However, the Applicant noticed that the decrease of the Mooney viscosity ML(1+4) of the elastomeric composition does not solve the drawbacks
25 mentioned above: the elastomeric composition still have the above reported drawbacks when extruded at high shear rates.

The Applicant then realized that, in order to operate at high shear rates, it was necessary to decrease
30 the elongational viscosity of said elastomeric composition. It should be noted that Mooney viscosity ML(1+4) and elongational viscosity are different properties as demonstrated, for example, by the fact that a decreasing of the Mooney viscosity ML(1+4) is not
35 always correlated with a decreasing of the elongational viscosity and viceversa.

The Applicant has now found that it is possible to

overcome the drawbacks mentioned above utilizing an elastomeric composition comprising at least one elongational viscosity reducing additive. The reduction of the elongational viscosity of the elastomeric composition allows to extrude an elastomeric elongated element at high shear rates and, consequently, allows to increase both the productivity of said elastomeric elongated elements and the process for producing a tyre in its entirety. Moreover, said additive does not negatively affect the mechanical properties, both tensile (in particular stress at break) and dynamic (in particular modulus and tandelta), as well as the kinetics of curing, of the elastomeric composition.

According to a first aspect, the present invention thus relates to a process for producing a tyre, which includes:

- feeding an elastomeric composition to an extruder;
- forming by extrusion said elastomeric composition as a continuous elongated element;
- depositing said continuous elongated element on a rigid support in a plurality of coils to make up a structural element of a tyre;

wherein the step of forming is carried out at a shear rate of at least 1000 s^{-1} and the elastomeric composition comprises at least one elongational viscosity reducing additive in an amount so that elongational viscosity of said elastomeric composition, measured at 120°C , at the shear rate of the forming step, is at least 10% lower with respect to the elongational viscosity, measured in the same conditions, of the elastomeric composition devoid of said additive.

According to one preferred embodiment, the elongational viscosity of said elastomeric composition, measured at 120°C , at the shear rate of the forming step, is 15% lower with respect to the elongational viscosity, measured in the same conditions, of the elastomeric composition devoid of said additive.

According to a further preferred embodiment, the elongational viscosity of said elastomeric composition, measured at 120°C, at the shear rate of the forming step, is not lower than 50% with respect to the elongational viscosity, measured in the same conditions, of the elastomeric composition devoid of said additive.

Preferably, said rigid support has a toroidal shape.

Preferably, said rigid support is a rotating support.

Preferably, said continuous elongated element is constituted by a strip of the elastomeric composition with flattened section such as, for example, rectangular, elliptic or lenticular, or also with a tapered shape. Cross-section dimensions of said strip are considerably lower than the cross-section dimensions of the structural element to be manufactured. By way of example, the continuous elongated element may have a width indicatively ranging between 3 mm and 15 mm and a thickness indicatively ranging between 0.5 mm and 1.2 mm.

Preferably, said coils are disposed side by side along the cross section profile of the rigid support. Said coils may be partially overlapped.

According to one preferred embodiment, said process is carried out with a drawing ratio (K) higher than 1, preferably higher than 1.5.

Said drawing ratio (K) is defined as the ratio between the deposition rate of the continuous elongated element and the production rate of the continuous elongated element. The deposition rate corresponds to the length of the elongated element deposited per time unit, as the production rate corresponds to the length of the elongated element produced per time unit.

According to a preferred embodiment, said forming step is carried out at a shear rate of between 2000 s⁻¹ and 8000 s⁻¹, preferably between 4000 s⁻¹ and 6000 s⁻¹.

According to a further aspect, the present invention relates to a method for reducing the elongational viscosity of an elastomeric composition which comprises

to add to said elastomeric composition at least one elongational viscosity reducing additive in an amount so that elongational viscosity of said elastomeric composition, measured at 120°C, at a shear rate of at least 1000 s⁻¹, is at least 10% lower with respect to the elongational viscosity, measured in the same conditions, of the elastomeric composition devoid of said additive.

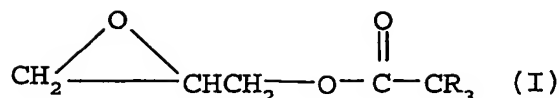
According to one preferred embodiment, the elongational viscosity of said elastomeric composition, measured at 120°C, at a shear rate of at least 1000 s⁻¹, is 15% lower with respect to the elongational viscosity, measured in the same conditions, of the elastomeric composition devoid of said additive.

According to a further preferred embodiment, the elongational viscosity of said elastomeric composition, measured at 120°C, at a shear rate of at least 1000 s⁻¹, is not lower than 50%, with respect to the elongational viscosity, measured in the same conditions, of the elastomeric composition devoid of said additive.

According to a further preferred embodiment said elongational viscosity reducing additive may be selected from:

- (a) glycidyl esters of an α -branched carboxylic acid containing from 6 to 22 carbon atoms;
- (b) polyolefin waxes;
- (c) copolymers of ethylene with at least one aliphatic α -olefin, and optionally a polyene;
- (d) thermoplastic polymers having a main hydrocarbon chain to which hydrophilic groups are linked;
- (e) fatty acid esters derived from at least one saturated or unsaturated fatty acid having from 8 to 24 carbon atoms and at least one polyhydric alcohol having from 2 to 6 carbon atoms.

According to one preferred embodiment, the glycidyl esters (a) may be selected from those having the following general formula (I):



wherein the R groups, equal or different from each others, represent hydrogen or linear or branched aliphatic groups, with the proviso that the R groups have a total number of carbon atoms of from 6 to 18, preferably from 8 to 12.

Said glycidyl esters (a) may be obtained by reacting a monofunctional α -branched carboxylic acid such as, for example, alkanolic acid (e.g. octanoic acid) or neoalkanoic acids (e.g. neodecanoic acid), with an epihalohydrin (e.g. epichlorohydrin), under conditions well known in the art. The glycidyl esters (a) of a neoalkanoic acid or of a mixture of neoalkanoic acids are particularly preferred.

Example of a glycidyl ester (a) which may be used in the present invention and which is currently commercially available is the product GlydexxTM N-10 from Exxon Mobil Chemical.

According to one preferred embodiment, the polyolefin waxes (b) may be selected from homopolymers of an α -olefin or copolymers of at least two α -olefin such as, for example, ethylene, propylene, 1-butene, 1-hexene, 4-methyl-1-pentene, 1-decene, or mixtures thereof, having an intrinsic viscosity (η), measured at 135°C in decalin, of between 0.03 dl/g to 1.0 dl/g.

Preferably, said polyolefin waxes (b) have the following characteristic:

- a molecular weight distribution (MWD) index of less than 5, preferably of between 1.0 and 3;
- a number-average molecular weight of less than 4000, preferably of between 450 and 3000;
- a melting point (T_m) of less than 140°C, preferably of between 70°C and 135°C,

- a viscosity at 140°C, measured according to ASTM standard D3236-88, of less than 160 cps, preferably of between 20 cps and 100 cps.

Said molecular weight distribution index is defined
5 as the ratio between the weight-average molecular weight (M_w) and the number-average molecular weight (M_n) and may be determined according to conventional techniques such as, for example, by means of gel permeation chromatography (GPC).

10 Polyolefin waxes (b) which may be used according to the present invention may be selected, for example, from: polyethylene wax obtained by pyrolysis of a high molecular weight polyethylene; polyethylene wax obtained by radical polymerization of ethylene at a high pressure;
15 polyethylene wax obtained by medium, low pressure polymerization of ethylene with the α -olefin mentioned above in the presence of a transition metal catalyst; polyethylene wax; ethylene/ α -olefin copolymer waxes; polypropylene wax; poly-1-butene wax; or mixtures
20 thereof. Polyethylene wax, or ethylene/ α -olefin copolymer waxes, are particularly preferred.

Examples of polyolefin waxes (b) which may be used in the present invention and which are currently commercially available are the products SP94 and SP96
25 from Baslini S.p.A.

According to one preferred embodiment, said at least one copolymer of ethylene (c), has a molecular weight distribution (MWD) index of less than 5, preferably between 1.5 and 3.5, and a melting enthalpy (ΔH_m) of not
30 less than 30 J/g, preferably between 34 J/g and 130 J/g.

Said molecular weight distribution index is defined as the ratio between the weight-average molecular weight (M_w) and the number-average molecular weight (M_n) and may be determined according to conventional techniques such
35 as, for example, by means of gel permeation chromatography (GPC).

Said melting enthalpy (ΔH_m) may be determined by Differential Scanning Calorimetry and relates to the melting peaks detected in the temperature range from 0°C to 200°C.

5 With reference to the copolymer of ethylene (c), the term "aliphatic α -olefin" generally means an olefin of formula $\text{CH}_2=\text{CH}-\text{R}$, in which R represents a linear or branched alkyl group containing from 1 to 12 carbon atoms. Preferably, the aliphatic α -olefin is selected
10 from propylene, 1-butene, isobutylene, 1-pentene, 4-methyl-1-pentene, 1-hexene, 1-octene, 1-dodecene, or mixtures thereof. 1-octene is particularly preferred.

With reference to the copolymer of ethylene (c), the term "polyene" generally means a conjugated or non-
15 conjugated diene, triene or tetraene. When a diene comonomer is present, this comonomer generally contains from 4 to 20 carbon atoms and is preferably selected from: linear conjugated or non-conjugated diolefins such as, for example, 1,3-butadiene, 1,4-hexadiene, 1,6-
20 octadiene, and the like; monocyclic or polycyclic dienes such as, for example, 1,4-cyclohexadiene, 5-ethylidene-2-norbornene, 5-methylene-2-norbornene, vinylnorbornene, or mixtures thereof. When a triene or tetraene comonomer is present, this comonomer generally contains from 9 to 30
25 carbon atoms and is preferably selected from trienes or tetraenes containing a vinyl group in the molecule or a 5-norbornen-2-yl group in the molecule. Specific examples of triene or tetraene comonomers which may be used in the present invention are: 6,10-dimethyl-1,5,9-undecatriene,
30 5,9-dimethyl-1,4,8-decatriene, 6,9-dimethyl-1,5,8-decatriene, 6,8,9-trimethyl-1,6,8-decatriene, 6,10,14-trimethyl-1,5,9,13-pentadecatetraene, or mixtures thereof. Preferably, the polyene is a diene.

According to another preferred embodiment, said
35 copolymer of ethylene (c) is characterized by:

- a density of between 0.86 g/cm³ and 0.93 g/cm³, preferably between 0.86 g/cm³ and 0.89 g/cm³;

- a Melt Flow Index (MFI), measured according to ASTM standard D1238-00, of between 0.1 g/10 min and 35 g/10 min, preferably between 0.5 g/10 min and 20 g/10 min;
- 5 - a melting temperature (T_m) of not less than 30°C, preferably between 50°C and 120°C, even more preferably between 55°C and 110°C.

The copolymer of ethylene (c) generally has the following composition: 50 mol%-98 mol%, preferably 60
10 mol%-93 mol%, of ethylene; 2 mol%-50 mol%, preferably 7 mol%-40 mol%, of an aliphatic α -olefin; 0 mol%-5 mol%, preferably 0 mol%-2 mol%, of a polyene.

The copolymer of ethylene (c) may be obtained by copolymerization of ethylene with an aliphatic α -olefin,
15 in the presence of a single-site catalyst such as, for example, a metallocene catalyst or of a constrained geometry catalyst.

Metallocene catalysts which may be used in the polymerization of olefins are, for example, coordination
20 complexes between a transition metal, usually from group IV, in particular titanium, zirconium or hafnium, and two optionally substituted cyclopentadienyl ligands, which are used in combination with a co-catalyst, for example an aluminoxane, preferably methylaluminoxane, or a boron
25 compound (see, for example, Adv. Organomet. Chem, Vol. 18, p. 99, (1980); Adv. Organomet. Chem, Vol. 32, p. 325, (1991); J.M.S. - Rev. Macromol. Chem. Phys., Vol. C34(3), pp. 439-514, (1994); J. Organometallic Chemistry, Vol. 479, pp. 1-29, (1994); Angew. Chem. Int., Ed. Engl., Vol.
30 34, p. 1143, (1995); Prog. Polym. Sci., Vol. 20, p. 459 (1995); Adv. Polym. Sci., Vol. 127, p. 144, (1997); patent US 5 229 478, or patent applications WO 93/19107, EP 35 342, EP 129 368, EP 277 003, EP 277 004, EP 632 065).

35 Constrained geometry catalysts which may be used in the polymerization of olefins are, for example, coordination complexes between a metal, usually from

groups 3-10 or from the Lanthanide series, and a single, optionally substituted cyclopentadienyl ligand, which are used in combination with a co-catalyst, for example an aluminoxane, preferably methylaluminoxane, or a boron compound (see, for example, Organometallics, Vol. 16, p. 3649, (1997); J. Am. Chem. Soc., Vol. 118, p. 13021, (1996); J. Am. Chem. Soc., Vol. 118, p. 12451, (1996); J. Organometallic Chemistry, Vol. 482, p. 169, (1994); J. Am. Chem. Soc., Vol. 116, p. 4623, (1994); Organometallics, Vol. 9, p. 867, (1990); patents US 5 096 867, US 5 414 040, or patent applications WO 92/00333, WO 97/15583, WO 01/12708, EP 416 815, EP 418 044, EP 420 436, EP 514 828.

The synthesis of the copolymers of ethylene (c) in the presence of metallocene catalysts is described, for example, in patent application EP 206 794, or in Metallocene-based polyolefins, Vol. 1, Wiley series in Polymer Science, p. 309, (1999).

The synthesis of copolymers of ethylene (c) in the presence of constrained geometry catalysts is described, for example, in Macromol. Chem. Rapid. Commun., Vol. 20, p. 214-218, (1999); Macromolecules, Vol. 31, p. 4724 (1998); Macromolecules Chem. Phys., Vol. 197, p. 4237 (1996); or in patent application WO 00/26268; or in patent US 5 414 040.

Examples of copolymers of ethylene (c) which may be used in the present invention and which are currently commercially available are the products Engage® from DuPont-Dow Elastomers and Exact® from Exxon Chemical.

With reference to the thermoplastic polymers (d), in the present description and claims, by the expression "thermoplastic polymer having a main hydrocarbon chain to which hydrophilic groups are linked" [for the sake of brevity also "hydrophilic polymer (d)"] it is meant a synthetic polymer wherein hydrophilic groups, either directly or through side groups, are linked to the main hydrocarbon chain, either linear or branched, and free

from glycoside bonds. As known, glycoside bonds are ether bonds, cleavable by hydrolysis, deriving from polycondensation of monosaccharides, which are typically present in polysaccharides such as starch and cellulose.

5 In the present description and claims, by "hydrophilic groups" it is meant groups which are able to bind water molecules by means of hydrogen bonds.

According to one preferred embodiment, said hydrophilic groups may be selected, for example, from:

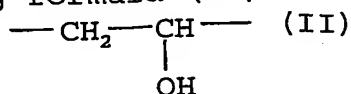
- 10 - hydroxyl groups -OH;
- carboxylic groups -COOH, possibly at least partially in the salt form;
- ester groups -COOR (R = alkyl or hydroxyalkyl);
- amide groups -CONH₂;
- 15 - sulfonic groups -SO₃H, possibly at least partially in the salt form.

Preferably, the hydrophilic polymers (d) according to the present invention are capable to absorb at least 0.1% by weight of water based on the polymer weight, after a
20 24-hour exposure in an environment having a 50% relative humidity at the temperature of 24°C (measured according to ASTM standard D570).

Preferably, the hydrophilic polymers (d) according to the present invention are thermoplastic products having a
25 melting temperature lower than 230°C, preferably between 200°C and 130°C.

According to one preferred embodiment, the hydrophilic polymers (d) may be selected, for example, from: polyacrylic acid, polymethacrylic acid,
30 polyhydroxyalkylacrylate, polyalkylacrylate, polyacrylamide, acrylamide/acrylic acid copolymers, polyvinylalcohol, polyvinylacetate, vinylalcohol/vinylacetate copolymers, ethylene/vinylacetate copolymers, ethylene/vinylalcohol
35 copolymers, ethylene/vinylalcohol/vinylacetate terpolymers, polyvinyl-sulfonic acid, polystyrene sulfonate, or mixtures thereof.

According to a particularly preferred embodiment, said hydrophilic polymers (d) comprise repeating units having the following formula (II):



5 with a random or block distribution along the chain.

This preferred class of hydrophilic polymers (d) encompasses: polyvinylalcohol, ethylene/vinylalcohol copolymers, ethylene/vinylalcohol/vinylacetate terpolymers. Polymers may also be used wherein the groups
10 of formula (II) have been at least partially modified, for instance by partial acetylation with aliphatic aldehydes (as described, for example, in patent US 4 002 796).

The following hydrophilic polymers (d) are
15 particularly preferred:

- (i) vinylalcohol polymers obtained by hydrolysis of polyvinylacetate, with a hydrolysis degree comprised between 50 mol% and 100 mol%, preferably between 70 mol% and 90 mol%;
- 20 (ii) ethylene/vinylalcohol copolymers having a content of ethylene units generally comprised between 20 mol% and 60 mol%, preferably between 25 mol% and 50 mol%.

Examples of copolymers of type (i) which may be used
25 in the present invention and which are currently commercially available are the products Mowiol[®] from Clariant, Gohsenol[®] from Nippon Gohsei, Elvanol[®] from Du Pont, Airvol[®] from Air Products.

Examples of copolymers of type (ii) which may be used
30 in the present invention and which are currently commercially available are the products Soarnol[®] from Atochem.

With regard to the fatty acid esters (e), the saturated fatty acid may be selected, for example, from:
35 capric acid, lauric acid, myristic acid, palmitic acid,

stearic acid, 12-hydroxystearic acid, behenic acid, or mixtures thereof. Stearic acid is preferred.

The unsaturated fatty acid may be selected, for example, from: undecylenic acid, oleic acid, erucic acid, sorbic acid, linoleic acid, linolenic acid, arachidonic acid, propiolic acid, stearolic acid, or mixtures thereof.

The polyhydric alcohol may be selected, for example, from: ethylene glycol, diethylene glycol, triethylene glycol, propylene glycol, dipropylene glycol, butanediol, pentanediol, hexanediol, glycerin, diglycerin, triglycerin, pentaerythritol, sorbitan, sorbitol, mannitol, or mixtures thereof. Glycerine is preferred.

Examples of fatty acid esters (e) which may be used in the present invention and which are currently commercially available are the products Ligalub[®] from Peter Greven Fett-Chemie.

The elongational viscosity reducing additives above disclosed may be added to the elastomeric composition according to the present invention as such or dispersed in a polymeric carrier so as to obtain a product in subdivided form (see, for example, the International Patent Application WO 02/083783 in the name of the same Applicant).

According to one preferred embodiment, the elongational viscosity reducing additive is present in the elastomeric composition in an amount of from 0.1 phr to 10 phr, preferably from 2 phr to 5 phr.

For the purposes of the present description and of the claims, the term "phr" means the parts by weight of a given component of the elastomeric composition per 100 parts by weight of the elastomeric polymer.

The elastomeric composition according to the present invention, also comprises at least one diene elastomeric polymer (f) which may be selected from those commonly used in sulphur-crosslinkable elastomeric compositions, that are particularly suitable for producing tyres, that

is to say from elastomeric polymers or copolymers with an unsaturated chain having a glass transition temperature (T_g) generally below 20°C , preferably in the range of from 0°C to -90°C . These polymers or copolymers may be of
5 natural origin or may be obtained by solution polymerization, emulsion polymerization or gas-phase polymerization of one or more conjugated diolefins, optionally blended with at least one comonomer selected from monovinylarenes and/or polar comonomers in an amount
10 of not more than 60% by weight.

The conjugated diolefins generally contain from 4 to 12, preferably from 4 to 8 carbon atoms, and may be selected, for example, from the group comprising: 1,3-butadiene, isoprene, 2,3-dimethyl-1,3-butadiene, 1,3-
15 pentadiene, 1,3-hexadiene, 3-butyl-1,3-octadiene, 2-phenyl-1,3-butadiene, or mixtures thereof. 1,3-butadiene and isoprene are particularly preferred.

Monovinylarenes which may optionally be used as comonomers generally contain from 8 to 20, preferably
20 from 8 to 12 carbon atoms, and may be selected, for example, from: styrene; 1-vinylnaphthalene; 2-vinylnaphthalene; various alkyl, cycloalkyl, aryl, alkylaryl or arylalkyl derivatives of styrene such as, for example, α -methylstyrene, 3-methylstyrene,
25 4-propylstyrene, 4-cyclohexylstyrene, 4-dodecylstyrene, 2-ethyl-4-benzylstyrene, 4-p-tolylstyrene, 4-(4-phenylbutyl)styrene, or mixtures thereof. Styrene is particularly preferred.

Polar comonomers which may optionally be used may be
30 selected, for example; from: vinylpyridine, vinylquinoline, acrylic acid and alkylacrylic acid esters, nitriles, or mixtures thereof, such as, for example, methyl acrylate, ethyl acrylate, methyl methacrylate, ethyl methacrylate, acrylonitrile, or
35 mixtures thereof.

Preferably, the diene elastomeric polymer (f) which may be used in the present invention may be selected, for

example, from: cis-1,4-polyisoprene (natural or synthetic, preferably natural rubber), 3,4-polyisoprene, polybutadiene (in particular polybutadiene with a high 1,4-cis content), optionally halogenated

5 isoprene/isobutene copolymers, 1,3-butadiene/acrylonitrile copolymers, styrene/1,3-butadiene copolymers, styrene/isoprene/1,3-butadiene copolymers, styrene/1,3-butadiene/acrylonitrile copolymers, or mixtures thereof.

10 The elastomeric composition according to the present invention may optionally comprise at least one elastomeric polymer of one or more monoolefins with an olefinic comonomer or derivatives thereof (g). The monoolefins may be selected from: ethylene and α -olefins
15 generally containing from 3 to 12 carbon atoms, such as, for example, propylene, 1-butene, 1-pentene, 1-hexene, 1-octene, or mixtures thereof. The following are preferred: copolymers between ethylene and an α -olefin, optionally with a diene; isobutene homopolymers or copolymers
20 thereof with small amounts of a diene, which are optionally at least partially halogenated. The diene optionally present generally contains from 4 to 20 carbon atoms and is preferably selected from: 1,3-butadiene, isoprene, 1,4-hexadiene, 1,4-cyclohexadiene, 5-
25 ethylidene-2-norbornene, 5-methylene-2-norbornene, vinylnorbornene, or mixtures thereof. Among these, the following are particularly preferred: ethylene/propylene copolymers (EPR) or ethylene/propylene/diene copolymers (EPDM); polyisobutene; butyl rubbers; halobutyl rubbers,
30 in particular chlorobutyl or bromobutyl rubbers; or mixtures thereof.

A diene elastomeric polymer (f) or an elastomeric polymer (g) functionalized by reaction with suitable terminating agents or coupling agents may also be used.

35 In particular, the diene elastomeric polymers obtained by anionic polymerization in the presence of an organometallic initiator (in particular an organolithium

initiator) may be functionalized by reacting the residual organometallic groups derived from the initiator with suitable terminating agents or coupling agents such as, for example, imines, carbodiimides, alkyltin halides, substituted benzophenones, alkoxysilanes or
5 aryloxysilanes (see, for example, European patent EP 451 604, or patents US 4 742 124 and US 4 550 142).

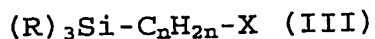
At least one reinforcing filler may advantageously be added to the elastomeric composition according to the
10 present invention, in an amount generally of from 0.1 phr to 120 phr, preferably from 20 phr to 90 phr. The reinforcing filler may be selected from those commonly used for crosslinked manufactured products, in particular for tyres, such as, for example, carbon black, silica,
15 alumina, aluminosilicates, calcium carbonate, kaolin, or mixtures thereof.

The types of carbon black which may be used according to the present invention may be selected from those conventionally used in the production of tyres, generally
20 having a surface area of not less than 20 m²/g (determined by CTAB absorption as described in ISO standard 6810).

The silica which may be used according to the present invention may generally be a pyrogenic silica or,
25 preferably, a precipitated silica, with a BET surface area (measured according to ISO standard 5794/1) of from 50 m²/g to 500 m²/g, preferably from 70 m²/g to 200 m²/g.

When a reinforcing filler comprising silica is present, the elastomeric composition may advantageously
30 incorporate at least one coupling agent capable of interacting with the silica and of linking it to the diene elastomeric polymer during the vulcanization.

Coupling agents that are preferably used are those based on silane which may be identified, for example, by
35 the following structural formula (III):



in which the groups R, which may be identical or

different, are selected from: alkyl, alkoxy or aryloxy groups or from halogen atoms, on condition that at least one of the groups R is an alkoxy or aryloxy group; n is an integer between 1 and 6 inclusive; X is a group
5 selected from: nitroso, mercapto, amino, epoxide, vinyl, imide, chloro, $-(S)_mC_nH_{2n}-Si-(R)_3$ in which m and n are integers between 1 and 6 inclusive and the groups R are defined as above.

Among the coupling agents that are particularly
10 preferred are bis(3-triethoxysilylpropyl) tetrasulphide and bis(3-triethoxysilylpropyl) disulphide. Said coupling agents may be used as such or as a suitable mixture with an inert filler (for example carbon black) so as to facilitate their incorporation into the elastomeric
15 composition.

The elastomeric composition according to the present invention may be vulcanized according to known techniques, in particular with sulphur-based vulcanizing systems commonly used for diene elastomeric polymers.

20 The vulcanizing agent most advantageously used is sulphur, or molecules containing sulphur (sulphur donors), with accelerators and activators known to those skilled in the art.

Activators that are particularly effective are zinc
25 compounds, and in particular ZnO, ZnCO₃, zinc salts of saturated or unsaturated fatty acids containing from 8 to 18 carbon atoms, such as, for example, zinc stearate, which are preferably formed in situ in the elastomeric composition from ZnO and fatty acid, and also BiO, PbO,
30 Pb₃O₄, PbO₂, or mixtures thereof.

Accelerators that are commonly used may be selected from: dithiocarbamates, guanidine, thiourea, thiazoles, sulphenamides, thiurams, amines, xanthates, or mixtures thereof.

35 The elastomeric composition according to the present invention may comprise other commonly used additives selected on the basis of the specific application for

which the composition is intended. For example, the following may be added to said composition: antioxidants, anti-ageing agents, adhesives, anti-ozone agents, modifying resins, fibres (for example Kevlar® pulp), or mixtures thereof.

The process for preparing a crosslinkable elastomeric composition according to the present invention may be carried out continuously or discontinuously.

When said process is carried out continuously, the mixing of the diene elastomeric polymer (f) with the elongational viscosity reducing additive and with the other components optionally present is carried out, for example, in continuous mixers such as a Ko-Kneader mixer (Buss) or in co-rotating or counter-rotating twin-screw extruders or in single-screw extruders.

When the process is carried out discontinuously, the mixing of the diene elastomeric polymer (f) with the elongational viscosity reducing additive and with the other components optionally present is carried out, for example, using an open internal mixer such as an open mill, or an internal mixer of the type with tangential rotors (Banbury) or with interlocking rotors (Intermix).

During the mixing, the temperature is kept below a predetermined value so as to avoid premature crosslinking of the composition. To this end, the temperature is generally kept below 170°C, preferably below 150°C, even more preferably below 120°C. As regards the mixing time, this may vary within a wide range, depending mainly on the specific composition of the mixture, on the presence of reinforcing fillers and on the type of mixer used. In general, a mixing time of more than 10 seconds, preferably between 30 seconds and 35 minutes is sufficient to obtain a homogeneous composition.

The present invention will now be illustrated in further detail by means of a number of illustrative embodiments, with reference to the attached Fig. 1 which is a view in cross section of a portion of a tyre made

according to the invention.

With reference to Fig. 1, the tyre (101) essentially comprises a carcass structure (102) having at least a first carcass ply (103) shaped in a substantially toroidal configuration and engaged, by means of its opposite circumferential edges, to a pair of inextensible annular structures (104) commonly known as "bead wires" which, once the tyre is finished, are located in the zone usually referred to as the bead. The opposite lateral edges of the abovementioned carcass ply (103) are coupled with respective bead wires (104). Alternatively, coupling between the carcass ply (103) and the bead wires (104) may be achieved by folding back the opposite lateral edges of the carcass ply (103) around the bead wires (104), so as to form the abovementioned carcass back-folds (not shown in Fig. 1).

The carcass ply (103) generally consists of a plurality of reinforcing cords arranged parallel to each other and at least partially coated with a layer of elastomeric material. These reinforcing cords are usually made of textile fibres, for example rayon, nylon or polyethylene terephthalate, or of steel wires which are stranded together, coated with a metal alloy (for example copper/zinc, zinc/manganese or zinc/molybdenum/cobalt alloys, and the like).

The carcass ply (103) is usually of radial type, i.e. it incorporates reinforcing cords arranged in a substantially perpendicular direction relative to a circumferential direction.

A belt structure (105) comprising one or more belt strips (106a), (106b) and (107) is applied to the carcass structure (102), in a circumferentially external position. In the specific embodiment of Fig. 1, the belt structure (105) comprises two belt strips (106a) and (106b), which incorporate a plurality of reinforcing cords, typically metal cords, parallel to each other in each strip and oblique with respect to the adjacent

strip, oriented so as to form a predetermined angle with respect to a circumferential direction. The belt structure (105) may optionally comprise at least one reinforcing layer (107) at 0° commonly known as a "0° belt", placed on the radially outermost belt strip (106b), which generally incorporates a plurality of reinforcing cords, typically textile cords, arranged at an angle of a few degrees with respect to a circumferential direction, coated and welded together by means of an elastomeric material.

A tread band (108) is superimposed circumferentially on the belt structure (105) and on it, after a moulding operation carried out concomitantly with the curing of the tyre, are made longitudinal and/or transverse grooves (108) arranged so as to define a desired "tread pattern".

The tyre (100) also comprises a pair of sidewalls (109) applied laterally to the opposite sides of the carcass structure (102). A strip made of elastomeric material (not shown in Fig. 1) commonly known as a "mini-sidewall" may optionally be present in the connecting zone between the sidewalls (109) and the tread band (108), which is generally obtained by co-extrusion with the tread band and makes it possible to improve the mechanical interaction between the tread band (108) and the sidewalls (109).

In the case of tubeless tyres, a further coating layer (not shown in Fig. 1) may also be provided in a radially internal position with respect to the carcass ply (103), over the coating layer (110) according to the present invention. This further coating layer can further ensure impermeability to a fluid for inflating the tyre when this tyre is installed on a rim and inflated.

The present invention will be further illustrated below by means of a number of preparation examples, which are given for purely indicative purposes and without any limitation of this invention.

EXAMPLES 1-3

Preparation of the elastomeric compositions

The elastomeric compositions given in Table 1 (the amounts of the different components are expressed in phr) were prepared as follows.

- 5 All ingredients, except sulphur and accelerators, were mixed in an internal mixer (Pomini PL 1.6 model) for about 5 minutes (1st Step). As soon as the temperature of $145 \pm 5^\circ$ was reached, the elastomeric composition was discharged. The sulphur and the accelerators were then
- 10 added and mixing was carried out in an open mill mixer equipped with cylinders (2nd Step).

TABLE 1

EXAMPLE	1 (*)	2	3
1 st STEP			
S-SBR	90	90	90
BR	35	35	35
Silica	70	70	70
Zinc oxide	2.5	2.5	2.5
TESPT	5.6	5.6	5.6
Stearic acid	2	2	2
Aromatic oil	8	8	8
Microcrystalline wax	1	1	1
Antioxidant	2	2	2
Glydexx [®] N-10	-	3	-
SP94	-	-	4
2 nd STEP			
CBS	2	2	2
DPG	1.9	1.9	1.9
Sulphur	1.2	1.2	1.2

(*): comparative.

- 5 S-SBR: styrene/butadiene copolymer, obtained by solution polymerization, containing 25% by weight of styrene, mixed with 37.5 phr of oil (Buna[®] 5025 - Bayer);
- BR: cis-1,4-polybutadiene (Europrene[®] BR 40 - EniChem Elastomeri);
- 10 Silica: precipitated silica (Zeosil[®] 1165 MP - Rhône-Poulenc);

TESPT: bis(3-triethoxysilylpropyl)tetrasulfide (X50S comprising 50% of carbon black and 50% of silane - Degussa-Hüls - the reported amount relates to the silane amount);

- 5 Antioxidant: N-1,3-dimethylbutyl-N'-phenyl-p-phenylenediamine;
Glydexx[®] N-10: glycidyl neodecanoate (Exxon Mobil Chemical);
SP94: polyethylene wax from Baslini S.p.A.;
- 10 CBS (accelerator): N-cyclohexyl-2-benzotiazyl-sulfenamide (Vulkacit[®] CZ - Bayer);
DPG (accelerator): N-N'-diphenylguanidine.

The Mooney viscosity ML(1+4) at 100°C was measured, according to ISO standard 289/1, on the non-crosslinked compositions obtained as described above. The results
15 obtained are given in Table 2.

Said elastomeric compositions were also submitted to a MDR rheometric analysis using a MDR rheometer from Monsanto, the tests being run at 170°C for 20 minutes,
20 with an oscillation frequency of 1.66 Hz (100 oscillations per minute) and an oscillation amplitude of $\pm 0.5^\circ$ (curing properties). The static mechanical properties according to ISO standard 37 as well as hardness in IRHD degrees at 23°C and at 100°C according
25 to ISO standard 48 were measured on samples of said elastomeric compositions cross-linked at 170°C for 10 minutes. The results obtained are given in Table 2.

Also given in Table 2 are the dynamic mechanical properties measured using an Instron dynamic device in
30 the traction-compression mode according to the following methods. A test piece of the crosslinked material having a cylindrical form (length = 25 mm; diameter = 14 mm) compression-preloaded up to 10% longitudinal deformation with respect to the initial length and kept at the
35 prefixed temperature (23°C or 70°C) for the whole duration of the test, was submitted to a dynamic sinusoidal strain with an amplitude $\pm 3.33\%$ with respect

to the length under pre-load, with a frequency of 100 Hz. The dynamic mechanical properties are expressed in terms of dynamic elastic modulus (E') and $\tan\delta$ (loss factor) values. As is known, the $\tan\delta$ value is
5 calculated as a ratio between the viscous modulus (E'') and the elastic modulus (E'), both of them being determined with the above dynamic measurements.

Also given in Table 2 are the elongational viscosities measured according to ASTM standard D5099-93
10 as follows.

The compositions obtained as disclosed above were subjected to capillary rheometric analysis using a Göttert laboratory rheometer Rheograph 6000 type equipped with three capillaries having 1 mm internal
15 diameter and different lengths: 10 mm; 20 mm and 30 mm, respectively. For this purpose, test pieces of the composition having a cylindrical form (length = 50 cm; diameter = 6 mm) were obtained by extrusion utilizing a Bandera laboratory extruder Garvey type having a
20 length/diameter ratio $L/D = 10$ and a twin screw speed of 80 rpm. The extruder was thermostated at 90°C.

The obtained test pieces, three for each elastomeric compositions, were pushed by means of a piston in the three capillaries, operating at a temperature of 120°C,
25 at a predetermined shear rates (the shear rates values (s^{-1}) are given in Table 2): the elongational viscosity was measured and the average of the three measures was given in Table 2.

TABLE 2

EXAMPLE	1 (*)	2	3
Mooney viscosity ML (1+4)	77	59	64
STATIC MECHANICAL PROPERTIES			
Stress at break (MPa)	15.4	14.7	14.0
Elongation at break (%)	399	414	386
DYNAMIC MECHANICAL PROPERTIES			
E' (23°C)	8.1	8.2	7.5
E' (70°C)	5.8	5.9	5.4
Tandelta (23°C)	0.264	0.272	0.272
Tandelta (70°C)	0.131	0.113	0.129
CURING PROPERTIES			
MH (dN m)	20.1	20.5	19.6
t30 (min)	1.8	1.9	1.8
t90 (min)	3.4	3.8	3.2
ELONGATIONAL VISCOSITY (Pa s)			
1786 s ⁻¹	339	278	285
2554 s ⁻¹	260	213	216
3711 s ⁻¹	195	172	162
5938 s ⁻¹	145	128	128
IRHD Hardness (23°C)	74	73	72
IRHD Hardness (100°C)	65	66	64

(*) : comparative.

Preparation of the elastomeric compositions

The elastomeric compositions given in Table 3 (the amounts of the various components are expressed in phr) were prepared by mixing together the elastomeric polymer (NR), the carbon black (N375) and the phenolic resin in a tangential internal mixer for about 5 minutes, reaching a final temperature of about 150°C. Next, said compositions were discharged from the internal mixer, introduced into a laboratory open-mill blender and the other components (given in Table 3) were added: the whole was mixed for about 3 minutes at 100°C.

TABLE 3

EXAMPLE	4 (*)	5	6
NR	100	100	100
N375	75	75	75
Zinc oxide	10	10	10
Stearic acid	2	2	2
Aromatic oil	2.4	2.4	2.4
Phenolic resin	18	18	18
Cobalt naphthenate	5.7	5.7	5.7
Antioxidant	1	1	1
SP94	-	4	-
Engage® 8150	-	-	4
TBBS	1	1	1
Sulphur	7	7	7
Retardant	0.4	0.4	0.4

(*): comparative.

15 NR: natural rubber;

N375: carbon black (Columbian);

Phenolic resin: octylphenolic resin (Durez[®] 29095 -
Occidental);

5 Adhesive: t-butylphenol formaldeide (Durez[®] 32333 -
Occidental);

Antioxidant: N-1,3-dimethylbutyl-N'-phenyl-p-
phenylenediamine;

SP94: polyethylene wax from Baslini S.p.A.;

10 Engage[®] 8150: ethylene/1-octene weight ratio = 75/25; d =
0.868 g/cm³; MFI = 0.5 g/10 min; ΔH_m = 34.8 J/g; T_m =
59.2°C) (Du Pont-Dow Elastomers);

TBBS (accelerator): N-t-butyl-2-benzotiazyl-
sulphenamide (Vulkacit[®] NZ - Bayer);

15 Retardant: cyclohexylthiophthalimide (Vulkalent[®] G -
Bayer).

The Mooney viscosity ML(1+4), the MDR rheometric
analysis (curing properties), the static mechanical
properties, as well as the elongational viscosities, were
measured operating as disclosed in Examples 1-3. The
20 results obtained are given in Table 4.

TABLE 4

EXAMPLE	4 (*)	5	6
Mooney viscosity ML (1+4)	121	105	114
STATIC MECHANICAL PROPERTIES			
Stress at break (MPa)	12.3	11.5	12.0
Elongation at break (%)	99.9	100.9	103.7
CURING PROPERTIES			
MH (dN m)	103.6	96.8	96.0
t ₃₀ (min)	2.21	2.23	2.20
t ₉₀ (min)	9.76	9.71	9.43
ELONGATIONAL VISCOSITY (Pa s)			
1456 s ⁻¹	615.7	525.0	550.0
1974 s ⁻¹	528.2	416.7	475.0
2986 s ⁻¹	454.4	330.0	401.2
4777 s ⁻¹	378.1	223.0	327.3
Shore D Hardness (23°C)	54	52	52
Shore D Hardness (100°C)	45	44	44

(*): comparative.

5 EXAMPLE 7

The elastomeric compositions of Example 1 (without elongational viscosity reducing additive) and Example 2 (according to the present invention) were fed to a single-screw extruder having a nominal screw diameter of 70 mm and a L/D ratio of 8.4, operating at an extrusion temperature of 130°C, at a shear rate of 5000 s⁻¹. Strips 25 mm wide and 3 mm thick were obtained which present:

- irregular edges and rough surface in the case of

Example 1;

- regular edges and smooth surface in the case of Example 2.

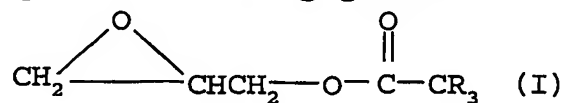
5 The strip obtained utilizing the elastomeric composition of Example 2 was used in order to make a tyre by means of a process according to the present invention.

CLAIMS

1. Process for producing a tyre, which includes:
 - 5 - feeding an elastomeric composition to an extruder;
 - forming by extrusion said elastomeric composition as a continuous elongated element;
 - 10 - depositing said continuous elongated element on a rigid support in a plurality of coils to make up a structural element of a tyre;wherein the step of forming is carried out at a shear rate of at least 1000 s^{-1} and the elastomeric composition comprises at least one elongational
15 viscosity reducing additive in an amount so that elongational viscosity of said elastomeric composition, measured at 120°C , at the shear rate of the forming step, is at least 10% lower with respect
20 to the elongational viscosity, measured in the same conditions, of the elastomeric composition devoid of said additive.
2. Process for producing a tyre according to claim 1, wherein the elongational viscosity of the elastomeric composition, measured at 120°C , at the shear rate of
25 the forming step, is 15% lower with respect to the elongational viscosity, measured in the same conditions, of the elastomeric composition devoid of said additive.
3. Process for producing a tyre according to claim 1 or
30 2, wherein the elongational viscosity of the elastomeric composition, measured at 120°C , at the shear rate of the forming step, is not lower than 50% with respect to the elongational viscosity, measured
35 in the same conditions, of the elastomeric composition devoid of said additive.
4. Process for producing a tyre according to any one of the preceding claims, wherein the rigid support has a

toroidal shape.

5. Process for producing a tyre according to any one of the preceding claims, wherein the rigid support is a rotating support.
- 5 6. Process for producing a tyre according to any one of the preceding claims, wherein the process is carried out with a drawing ratio (K) higher than 1.
7. Process for producing a tyre according to claim 6, wherein the drawing ratio (K) is higher than 1.5.
- 10 8. Process for producing a tyre according to any one of the preceding claims, wherein the forming step is carried out at a shear rate of between 2000 s^{-1} and 8000 s^{-1} .
9. Process for producing a tyre according to claim 8,
 - 15 wherein the forming step is carried out at a shear rate of between 4000 s^{-1} and 6000 s^{-1} .
10. Process for producing a tyre according to any one of the preceding claims, wherein the elongational viscosity reducing additive is selected from:
 - 20 (a) glycidyl esters of an α -branched carboxylic acid containing from 6 to 22 carbon atoms;
 - (b) polyolefin waxes;
 - (c) copolymers of ethylene with at least one aliphatic α -olefin, and optionally a polyene;
 - 25 (d) thermoplastic polymers having a main hydrocarbon chain to which hydrophilic groups are linked;
 - (e) fatty acid esters derived from at least one saturated or unsaturated fatty acid having from 8 to 24 carbon atoms and at least one polyhydric
 - 30 alcohol having from 2 to 6 carbon atoms.
11. Process for producing a tyre according to claim 10, wherein the glycidyl esters (a) are selected from those having the following general formula (I):



35 wherein the R groups, equal or different from each

others, represent hydrogen or linear or branched aliphatic groups, with the proviso that the R groups have a total number of carbon atoms of from 6 to 18.

12. Process for producing a tyre according to claim 10,
5 wherein the polyolefin waxes (b) are selected from homopolymers of an α -olefin or copolymers of at least two α -olefin such as ethylene, propylene, 1-butene, 1-hexene, 4-methyl-1-pentene, 1-decene, or mixtures thereof, having an intrinsic viscosity (η), measured
10 at 135°C in decalin, of between 0.03 dl/g to 1.0 dl/g.
13. Process for producing a tyre, according to claim 12, wherein the polyolefin waxes (b) have a molecular weight distribution (MWD) index of less than 5.
- 15 14. Process for producing a tyre, according to claim 12 or 13, wherein the polyolefin waxes (b) have a number-average molecular weight of less than 4000.
15. Process for producing a tyre, according to any one of claims 12 to 14, wherein the polyolefin waxes (b)
20 have a melting point (T_m) of less than 140°C.
16. Process for producing a tyre, according to any one of claims 12 to 15, wherein the polyolefin waxes (b) have a viscosity at 140°C, measured according to ASTM standard D3236-88, of less than 160 cps.
- 25 17. Process for producing a tyre, according to any one of claims 12 to 16, wherein the polyolefin waxes (b) are polyethylene wax, or ethylene α -olefin copolymer waxes.
18. Process for producing a tyre, according to claim 10,
30 wherein the copolymer of ethylene (c), has a molecular weight distribution (MWD) index of less than 5 and a melting enthalpy (ΔH_m) of not less than 30 J/g.
19. Process for producing a tyre according to claim 18,
35 wherein in the copolymer of ethylene (c) the aliphatic α -olefin is an olefin of formula $CH_2=CH-R$, in which R represents a linear or branched alkyl

group containing from 1 to 12 carbon atoms.

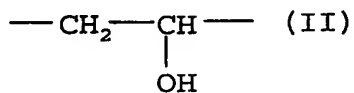
20. Process for producing a tyre according to claim 19,
wherein the aliphatic α -olefin is selected from
propylene, 1-butene, isobutylene, 1-pentene, 4-
5 methyl-1-pentene, 1-hexene, 1-octene, 1-dodecene, or
mixtures thereof.
21. Process for producing a tyre according to claim 20,
wherein the aliphatic α -olefin is 1-octene.
22. Process for producing a tyre according to any one of
10 claims 18 to 21, wherein the polyene is a conjugated
or non-conjugated diene, triene or tetraene.
23. Process for producing a tyre according to claim 22,
wherein the polyene is a diene.
24. Process for producing a tyre according to any one of
15 claims 18 to 23, wherein the copolymer of ethylene
(c) has a density of between 0.86 g/cm³ and 0.93
g/cm³.
25. Process for producing a tyre according to any one of
claims 18 to 24, wherein the copolymer of ethylene
20 (c) has a Melt Flow Index (MFI), measured according
to ASTM standard D1230-00, of between 0.1 g/10 min
and 35 g/10 min.
26. Process for producing a tyre according to any one of
claims 18 to 25, wherein the copolymer of ethylene
25 (c) has a melting point of not less than 30°C.
27. Process for producing a tyre according to claim 10,
wherein in the hydrophilic polymers (d) the
hydrophilic groups are selected from:
- hydroxyl groups -OH;
 - 30 - carboxylic groups -COOH, possibly at least
partially in the salt form;
 - ester groups -COOR (R = alkyl or hydroxyalkyl);
 - amide groups -CONH₂;
 - sulfonic groups -SO₃H, possibly at least
35 partially in the salt form.
28. Process for producing a tyre according to claim 27,
wherein the hydrophilic polymers (d) are capable of

absorbing at least 0.1% by weight of water based on the polymer weight after a 24-hour exposure in an environment having a 50% relative humidity at the temperature of 24°C (measured according to ASTM standard D570).

29. Process for producing a tyre according to claim 27 or 28, wherein the hydrophilic polymers (d) have a melting temperature lower than 230°C.

30. Process for producing a tyre according to any one of claims 27 to 29, wherein the hydrophilic polymers (d) are selected from: polyacrylic acid, polymethacrylic acid, polyhydroxy-alkylacrylate, polyalkylacrylate, polyacrylamide, acrylamide/acrylic acid copolymers, polyvinylalcohol, polyvinylacetate, vinylalcohol/vinylacetate copolymers, ethylene/vinylacetate copolymers, ethylene/vinylalcohol copolymers, ethylene/vinylalcohol/vinylacetate terpolymers, polyvinylsulfonic acid, polystyrene sulfonate, or mixtures thereof.

31. Process for producing a tyre according to any one of claims 27 to 30, wherein the hydrophilic polymers (d) comprise repeating units having the following formula (II):



with a random or block distribution along the chain.

32. Process for producing a tyre according to any one of claims 27 to 31, wherein the hydrophilic polymers (d) are selected from:

- (i) vinylalcohol polymers obtained by hydrolysis of polyvinylacetate, with a hydrolysis degree comprised between 50 mol% and 100 mol%;
- (ii) ethylene/vinylalcohol copolymers having a content of ethylene units comprised between 20 mol% and 60 mol%.

33. Process for producing a tyre according to claim 10,
wherein in the fatty acid esters (e), the saturated
fatty acid are selected from: capric acid, lauric
acid, myristic acid, palmitic acid, stearic acid, 12-
5 hydroxystearic acid, behenic acid, or mixtures
thereof.
34. Process for producing a tyre according to claim 33,
wherein the saturated fatty acid is stearic acid.
35. Process for producing a tyre according to claim 10,
10 wherein in the fatty acid esters (e), the unsaturated
fatty acid are selected from: undecylenic acid, oleic
acid, erucic acid, sorbic acid, linoleic acid,
linolenic acid, arachidonic acid, propiolic acid,
stearolic acid, or mixtures thereof.
- 15 36. Process for producing a tyre according to any one of
claim 33 to 35, wherein in the fatty acid esters (e),
the polyhydric alcohol may be selected from: ethylene
glycol, diethylene glycol, triethylene glycol,
propylene glycol, dipropylene glycol, butanediol,
20 pentanediol, hexanediol, glycerin, diglycerin,
triglycerin, pentaerythritol, sorbitan, sorbitol,
mannitol, or mixtures thereof.
37. Process for producing a tyre according to claim 36,
wherein the polyhydric alcohol is glycerine.
- 25 38. Process for producing a tyre according to any one of
the preceding claims, wherein the elongational
viscosity reducing additive is present in the
elastomeric composition in an amount of from 0.1 phr
to 10 phr.
- 30 39. Process for producing a tyre according to claim 38,
wherein the elongational viscosity reducing additive
is present in the elastomeric composition in an
amount of from 2 phr to 5 phr.
- 35 40. Process for producing a tyre according to any one of
the preceding claims, wherein the elastomeric
composition comprises at least one diene elastomeric
polymer (f).

41. Process for producing a tyre according to claim 40, wherein the diene elastomeric polymer (f) has a glass transition temperature (T_g) below 20°C.
- 5 42. Process for producing a tyre according to claim 41, wherein the diene elastomeric polymer (f) is selected from: cis-1,4-polyisoprene, 3,4-polyisoprene, polybutadiene, optionally halogenated isoprene/isobutene copolymers, 1,3-butadiene/acrylonitrile copolymers, styrene/1,3-butadiene copolymers, styrene/isoprene/1,3-butadiene copolymers, styrene/1,3-butadiene/acrylonitrile copolymers, or mixtures thereof.
- 10 43. Process for producing a tyre according to any one of the preceding claims, wherein the elastomeric composition comprises at least one elastomeric polymer of one or more monoolefins with an olefinic comonomer or derivatives thereof (g).
- 15 44. Process for producing a tyre according to claim 43; wherein the elastomeric polymer (g) is selected from: ethylene/propylene copolymers (EPR) or ethylene/propylene/diene copolymers (EPDM); polyisobutene; butyl rubbers; halobutyl rubbers; or mixtures thereof.
- 20 45. Process for producing a tyre according to any one of the preceding claims, wherein at least one reinforcing filler is present, in an amount of between 0.1 phr and 120 phr, in the elastomeric composition.
- 25 46. Process for producing a tyre according to claim 45, wherein the reinforcing filler is carbon black.
- 30 47. Process for producing a tyre according to claim 45, wherein the reinforcing filler is silica.
48. Process for producing a tyre according to claim 47, wherein at least one coupling agent is present.
- 35 49. Method for reducing the elongational viscosity of an elastomeric composition which comprises to add to said elastomeric composition at least one

elongational viscosity reducing additive in an amount so that elongational viscosity of said elastomeric composition, measured at 120°C, at a shear rate of at least 1000 s⁻¹, is at least 10% lower with respect to the elongational viscosity, measured in the same conditions, of the elastomeric composition devoid of said additive.

50. Method for reducing the elongational viscosity of an elastomeric composition according to claim 49, wherein the elongational viscosity of the elastomeric composition, measured at 120°C, at a shear rate of at least 1000 s⁻¹, is 15% lower with respect to the elongational viscosity, measured in the same conditions, of the elastomeric composition devoid of said additive.

51. Method for reducing the elongational viscosity of an elastomeric composition according to claim 49 or 50, wherein the elongational viscosity of the elastomeric composition, measured at 120°C, at a shear rate of at least 1000 s⁻¹, is not lower than 50% with respect to the elongational viscosity, measured in the same conditions, of the elastomeric composition devoid of said additive.

52. Method for reducing the elongational viscosity of an elastomeric composition according to any one of claims 49 to 51, wherein the elongational viscosity reducing additive is defined according to any one of claims 10 to 39.

53. Method for reducing the elongational viscosity of an elastomeric composition according to any one of claims 49 to 52, wherein the elastomeric composition comprises at least a diene elastomeric polymer (f) which is defined according to any one of claims 40 to 42.

54. Method for reducing the elongational viscosity of an elastomeric composition according to any one of claims 49 to 53, wherein the elastomeric composition

comprises at least one elastomeric polymer of one or more monoolefins with an olefinic comonomer or derivatives thereof (g) which is defined according to claim 43 or 44.

- 5 55. Method for reducing the elongational viscosity of an elastomeric composition according to any one of claims 49 to 54, wherein the elastomeric composition comprises at least one reinforcing filler, in an amount of between 0.1 phr and 120 phr.
- 10 56. Method for reducing the elongational viscosity of an elastomeric composition according to claim 55, wherein the reinforcing filler is defined according to any one of claims 46 to 48.

ABSTRACT

The present invention relates to a process for producing a tyre, which includes:

- 5 - feeding an elastomeric composition to an extruder;
- forming by extrusion said elastomeric composition as a continuous elongated element;
- depositing said continuous elongated element on a rigid support in a plurality of coils to make up a
- 10 structural element of a tyre;

wherein the step of forming is carried out at a shear rate of at least 1000 s^{-1} and the elastomeric composition comprises at least one elongational viscosity reducing additive in an amount so that elongational viscosity of

15 said elastomeric composition, measured at 120°C , at the shear rate of the forming step, is at least 10% lower with respect to the elongational viscosity, measured in the same conditions, of the elastomeric composition devoid of said additive.

20

Fig. 1

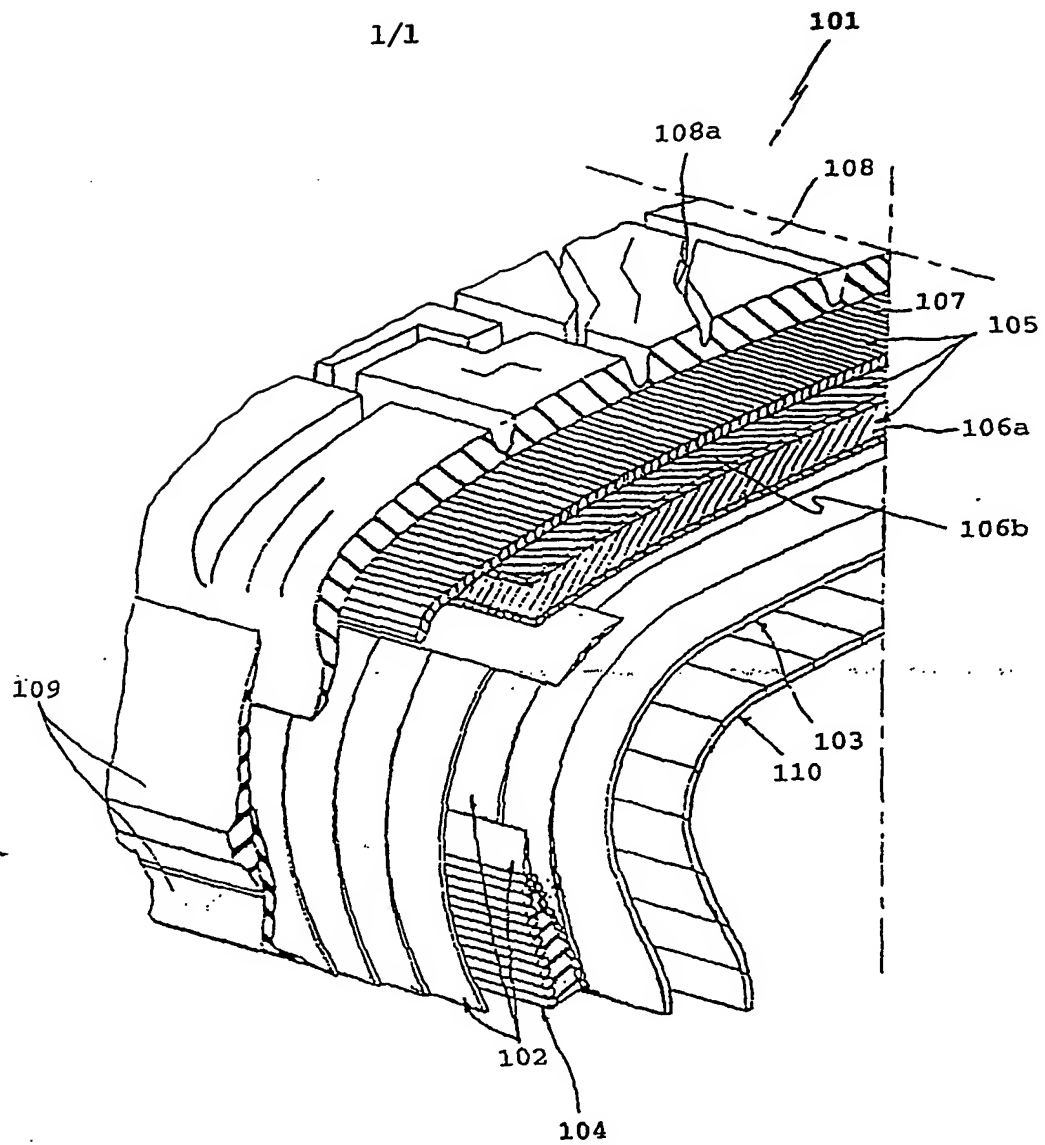


Fig. 1



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